

Biodiesel Production from Rubber Seed Oil with Transesterification Process

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Abstract

Diesel fuel needs are increasing with the depletion of petroleum reserves demanded to undertake the manufacture of alternatives fuels, one of which is biodiesel. Biodiesel fuel and fuel additive are derived from organic, renewable feed stocks. Rubber seed oil is one type of vegetable oil that can be processed into biodiesel. This research is conducted the trans-esterification process with variable mole ratio and reaction time. The first stage is the esterification process in order to reduce FFA level contained in the rubber seed oil to $\leq 2\%$. Ester which has been produced is processed into biodiesel by trans-esterification process using methanol solvent and KOH. The process of reacting ester and 50 ml of a 0.44 gr KOH (1% from the weight of ester) in a three-neck flask heated using water bath with temperature at 60°C and stirring speed 600 rpm. Variable used is mole variation, 1:4, 1:5 and 1:6 and the reaction time variations are 60, 120, and 180 minutes. Reaction products which has been formed is precipitated about ± 24 hours to separate the biodiesel with glycerol, and then washed it with water that has been heated by 10% of the total volume of biodiesel and separated again by using a funnel separator ± 24 hours. Biodiesel obtained was distilled to evaporate residual catalyst, soap and water. The density of biodiesel was tested in the laboratory of Technology Oil Gas and Coal Chemical Engineering Department, Faculty of Engineering, Gadjah Mada University. The results were obtained clear yellow biodiesel and glycerol as the other result. Optimal conditions obtained in the mole ratio variation is 1:5 with the results of biodiesel volume 48 ml, and the optimal condition at 60 minutes reaction time, the biodiesel volume produced is 96 % v.

Key Words: Biodiesel, rubber seed oil, trans-esterification,

1 Introduction

The increasing energy needs, led the use of fuel increases, this results the oil reserves are diminishing. These conditions encourage countries in the world for exploration to make an efficiency and diversification of fuel oil [1]. ROAD MAP according to the development of biofuels, the government plan 20% biodiesel used for consumption is 10.22 million kilo liters of diesel fuel [2,7]. Therefore this research on biodiesel was very prospective [3]. Biodiesel was composed from various fatty acid esters that can be produced from plant oils such as palm oil, coconut oil, castor oil and rubber seed oil. According [1], rubber seed is very potential raw material for biodiesel rubber seed oil. It contains 40 -50% of dry matter and FFA of FFA = 4.6%. Nowadays, the rubber is widely used. In addition, seeds can be taken from rubber seed and its meal oil [3]. Availability of rubber seeds is very high in Indonesia, because Indonesia is a country that produces largest rubber in the World. Based on the statistical data, extensive rubber plantations in Indonesia estimated about 3,318,105 ha and capable producing

rubber seed oil about 12,622,406.8 L / year. It has not been widely use rubber seeds [3]. The results rubber seed oil cannot be directly used as biodiesel, because the rubber seed oil contains of FFA (Free Fatty Acid). The FFA contained in the rubber seed should not exceed 2% to produce biodiesel. Trans-esterification process will not occur if the FFA in the oil is about 3%. Process carried out in order to decrease FFA. The FFA levels in rubber seeds are to decrease until to 2% so it can be processed into biodiesel [5]. Rubber seed oil contains saturated fatty acids and unsaturated fatty acids. Based on the chemical properties of rubber seed oil was non edible fat. Based on the physical properties results, it is showed that the rubber seed oil has properties so the oil could feasibly be used as raw material for the production of biodiesel feed stock [3].

Intake of rubber seed oil can be done by pressed and extracted with solvents. If the rubber seed is taken by pressing it, it will produce brownish yellow oil with a distinctive aroma. Besides that, the retrieval can be done by extracted rubber seed that results yellow bright oil, but less efficient if the oil needed in large quantities because of the time required for the extraction is longer [6].

The advantages of biodiesel are [1]: Have a higher cetane number (> 60) so the efficiency of combustion is better and reduce detonation or knock on the machine, have the lubrication properties to the piston engine. Biodegradable (decompose) is a renewable energy because it made of natural ingredients which renewable. The advantages from using rubber seed [6] which is renewable energy source, improve the economy of fuel, more economical, and environmentally friendly. According [8], esterification process is running slowly and irreversible. Trans-esterification reaction is a chemical process of exchanging alkoxy group of an ester compound with alcohol. Trans-esterification is the removal alcohol reaction from an ester by another alcohol which includes a series of three consecutive reversible reaction. The first reaction is conversion of triglycerides into diglycerides, conversion of diglycerides into monoglycerides, and the last is conversion of monoglycerides into glycerin. At each stage of the reaction produces esters (1). According to Salamah (20120), trans-esterification reaction lasts about 0.5-1 hour at a temperature 40°C until formed two layers. The bottom layer is glycerol and the top layer is methyl ester. Biodiesel synthesis through the trans-esterification reaction between oil composed of triglycerides with methanol molecules:



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2 Experimental

2.1 Analysis of Free Fatty Acid (FFA)

The rubber seed oil weight 10-20 grams. Neutral alcohol 96% was added and then heated in a water bath 10 minutes while stirring and cooling with a closed back cooling. After cooled and then titrated with 0.1 N KOH used the indicator was red phenolphthalein until the proper the solution guava red cooler.

2.2 Esterification process to decrease levels of FFA from the oil:

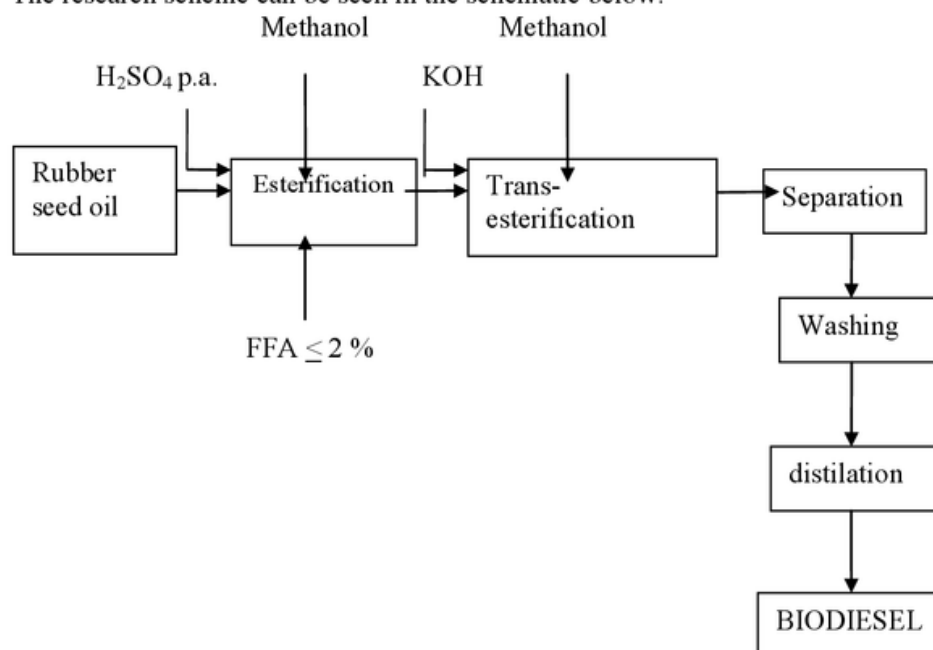
Setting up 19 rubber seed oil and methanol with mole ratio 1:6 and 1.5 N H₂SO₄, 1.5 from of rubber seed oil. Reacting the rubber seed oil, methanol and H₂SO₄, in three neck flask equipped with a cooling loop, stirrer, thermometer and water bath as heated. Reaction at 60 °C and stirring at 600 rpm for 60 minutes. Heating the reaction to remove methanol and water. The result FFA levels of esterificasi results obtained. If the FFA content of <2 then continue with the process of make biodiesel.

2.3 Trans-esterification Process

Take 50 ml of ester, add 18 ml of technically methanol which has been added with 0, 44 gr KOH (1% from the ester weight). The mixture was put into a three-neck flask and heat with water bath for 60 minutes at 60°C temperature and stirring speed 600 rpm. Put the result from trans-esterification process into a separator funnel and left it for 24 hours to complete the separation until formed two layers, the top layer is methyl ester (biodiesel) and bottom layer is glycerol. The experiment was repeated with variations of mole ratio (1:4, 1:5, 1:6) with vary amount of methanol and ester in accordance with the result of the mole ratio. The experiment was repeated with the same procedure with the variation time reaction 60, 120 and 180 minutes.

2.4 Research Scheme

The research scheme can be seen in the schematic below:



3 Result and Discussion

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3.1 Decrease of FFA (Free Fatty Acid) Rubber Seed Oil

Result FFA analysis of rubber seed oil obtained first FFA content 8.232%. After a decline with esterification process using H₂SO₄ concentrates FFA content 1.3067%, from this result is worth to manufacturing biodiesel process by using rubber seed oil.

3.2 The Influence of Material Mole Ratio

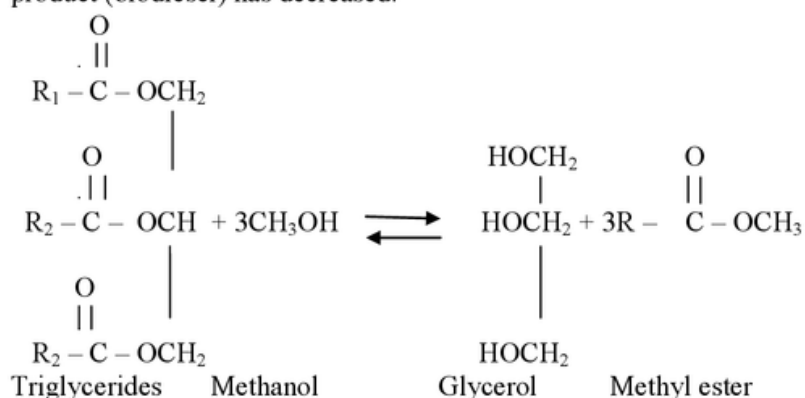
In the manufacture of biodiesel with mole ratio variable, this experiment done for about 60 minutes, stirring speed is 600 rpm, and the temperature is 60°C.

The following experimental data are presented in table 1:

Table.1 . The relationship between material mole ratio with biodiesel volume

No.	Mole Ratio	Volume Biodiesel Produced (ml)	Biodiesel (% V)
1.	1:4	36	72
2.	1:5	48	96
3.	1:6	44	88

From table 1 it can be known % of the optimum result of biodiesel volume is in mole ratio 1:5 with methanol reactant 18 ml and 50 ml of oil. Theoretically, the addition of methanol can increase the biodiesel result, but after reaching the optimum point decline % of result volume. It is because the trans-esterification reaction is reversible reaction. In this study indicates the equilibrium will shift to the left when the reaction has passed the optimum point so that the amount of product (biodiesel) has decreased.



3.3 The Influence of Reaction Time Variation

In this variable, the experiments done by using mole ratio 1:5 because this mole ratio can produce the highest volume of biodiesel. The following experimental data presented in figure 1:

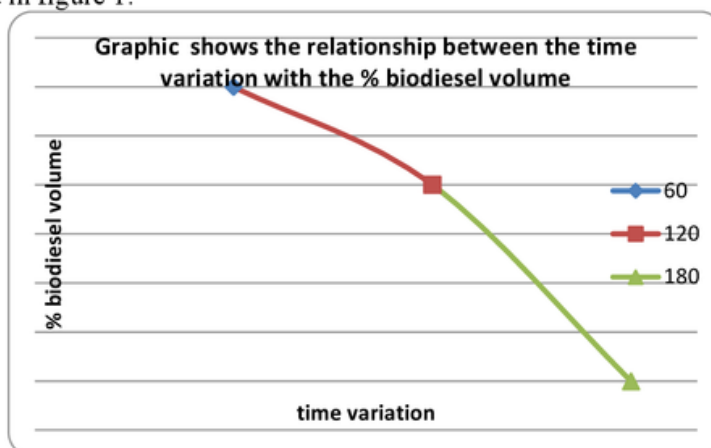


Figure 1 Graphic of the relationship between the time variations with % biodiesel volume

From figure 1 can be seen that the longer the time reaction, the less biodiesel volume. According [8], this is happen because the trans-esterification is a reversible reaction, to obtain a large biodiesel, then methanol that is given has to be excessive, naturally the methanol it self is volatile, so the length of reaction time will speed up evaporation as supported by relatively remained heat ($T = 60^{\circ}\text{C}$, the boiling point of methanol is $64,7^{\circ}\text{C}$). As the result, the amount of methanol to react with fatty acid decreased, this has resulted the biodiesel amount that is formed is also decreased.

The quality of biodiesel was tested in the laboratory of Oil Gas Technology and Coal Chemical Engineering Department, Faculty of Engineering, Gadjah Mada University, Yogyakarta, Indonesia. The result is the yellow colour of biodiesel from rubber seed oil quality is listed in Table 2:

Table 2. Physical properties of biodiesel

No	Property	Result Experiment	Experiment Method
1	Viscosity Kinematic at 40°C , mm ² /s	4,656	ASTM D 445-07
2	Flash Point PM.cc, $^{\circ}\text{C}$	164,5	ASTM D 93
3	Specific Gravity at 60/60 $^{\circ}\text{F}$, gr/ml	0,8856	ASTM D 1298
4	Cloud Point, $^{\circ}\text{C}$	6	ASTM D 97-07

Table 2 shows the research results obtained by biodiesel from rubber seed oil has properties. According to ISO quality standards of quality Biodiesel Indonesia (RSNI EB 020551).

The heat test result shows the result is 9520.684 Kal/gr. According [9] the major heat is a good size because it is above the heat on ISO standards, biodiesel heat in general is 9206 Kal/gr.

4 Conclusion

From the result of the research, the researchers could draw conclusion as follows:

1. The rubber seed oil can process to biodiesel with esterification process to be continue by transesterification process .
2. The optimum time reaction trans-esterification proces was 60 minute with biodiesel volume 48 ml. The optimum mole ratio was 1:5 with biodiesel 96% volume .

5 Reference

- [1] Sivaprakasam, S., Saravanan, C.G., (2007), "*Optimization of the Transesterification Process for Biodiesel Production and Use of Biodiesel in a Compression Ignition Engine*", Enerfy & Fuel jurnal, 21, page 2998-3003
- [2] TIMNAS BBN, (2008), "*Bahan Bakar alternatif dari tumbuhan sebagai pengganti minyak bumi dan gas*" Eka Cipta Fondation, penebar Swadaya, Jakarta
- [3] Salamah, S. (2012), Characterization of Rubber Seed Oil and The Decreased in the Value of FFA as a Introduction to Produce of Alternatife Fuels Biodiesel. Prosiding ISBN : 978-979-3812-25-0. Proceeding of International Conference on Green World in Business and Technology March 23-24, 2012. Ahmad lanUniversity Yogyakarta. (page 45-52)
- [4] Prihandana, R., Hendroko, R., (2007), "*Energi Hijau, Pilihan Bijak Menuju Energi Mandiri Energi*" Penebar Swadaya , Jakarta
- [5] Ramadhans, A.S., Mulareedharan, C., Jayaraj, S., 2005. "Performance and emission evaluation of diesel engine fueled with methyls esters of rubber seed oil", Renewable Energy, 30(2) 789-1800
- [6] Fitri Yuliani, dkk., 2009. "*Pengaruh Katalis Asam (H_2SO_4) dan Suhu Reaksi pada Reaksi Esterifikasi Minyak Biji Karet (*Hevea brasiliensis*) Menjadi Biodiesel*. Laboratorium Biomassa dan Energi, Institut Teknologi Sepuluh Nopember, Surabaya
- [7] Wiyarno, B., (2010), "*Biodiesel Microalgae, Bahan Bakar Alternatif Generasi ke tiga*", Era Pustaka utama , Solo, Indonesia
- [8] Fessenden R.j. Joan S. Fessenden, (1986) "Organic Chemistry" Jilid I dan II, Erlangga, Jakarta.
- [9] Soerawidjaja, T. H., 2003, *Standar Tentatif Biodiesel Indonesia dan Metode-metode Pengujiannya*, disampaikan dalam Diskusi Forum Biodiesel Indonesia, Bandung.

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| 8 | Ahmad, Junaid, Suzana Yusup, Awais Bokhari, and Ruzaimah Nik Mohammad Kamil. "Biodiesel Production from the High Free Fatty Acid <i>Hevea brasiliensis</i> and Fuel Properties Characterization", <i>Applied Mechanics and Materials</i> , 2014.
Crossref | 18 words — 1% |

-
- 9 M. Satyanarayana. "Comparative Studies of Biodiesel Production from Rubber Seed Oil, Coconut Oil, and Palm Oil Including Thermogravimetric Analysis", Energy Sources Part A Recovery Utilization and Environmental Effects, 01/2011
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- 15 Yang, R.. "Biodiesel production from rubber seed oil using poly (sodium acrylate) supporting NaOH as a water-resistant catalyst", Bioresource Technology, 201102
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- 16 www.faqs.org
Internet 12 words — 1%
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- 17 Ramadhas, A.S.. "Theoretical modeling and experimental studies on biodiesel-fueled engine", Renewable Energy, 200609
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development of rubber seed utilisation in Southeast Asia",
Clean Technologies and Environmental Policy, 2014.

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19 Ramadhas, A.S.. "Biodiesel production from high FFA rubber seed oil", Fuel, 200503 9 words — < 1%

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